



**SAFE OPERATION
OF AMMONIA
REFRIGERATION PLANT**

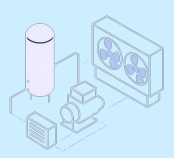
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HISTORY & EVOLUTION OF INDUSTRIAL AMMONIA REFRIGERATION

- 1850s**
Ferdinand Carré patents the first absorption refrigeration system using ammonia and water.
- Early 1900s**
NH₃ becomes the dominant refrigerant in industrial cold storage and food processing plants.
- 1970s-1990s**
Global standards emerge as plant scale increases and safety regulations tighten.
- 2000s-Present**
NH₃ reaffirmed as the preferred industrial refrigerant due to zero GWP/GWP and superior efficiency.

Today, the International Institute of Ammonia Refrigeration sets the global benchmark for design, operation, and safety of NH₃ systems, with guidelines adopted across food, pharmaceutical, and chemical industries worldwide.



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WHY INDUSTRIES PREFER AMMONIA (NH₃)

- High COP**
Ammonia has one of the highest Coefficients of Performance of any refrigerant, reducing energy costs significantly.
- Excellent Heat Transfer**
Superior thermal properties reduce heat exchanger size and improve overall system efficiency.
- Zero ODP & GWP**
NH₃ does not deplete the ozone layer and has zero global warming potential — fully compliant with all environmental protocols.
- Long Equipment Life**
Well-maintained NH₃ systems routinely operate for 25-40 years, delivering outstanding return on investment.

Property	NH ₃	CO ₂	R134a	R220A
ODP	0	0	0	0
GWP	0	1	1,430	3,522
COP	★★★★	★★	★★	★
Toxicity	Yes	No	No	No
Cost	Low	Medium	High	High

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HEALTH HAZARDS, EXPOSURE LIMITS & FIRST AID

Exposure Limits

Standard	Limit
Threshold Limit Value	25 ppm
Short-Term Exposure Limit	35 ppm (15 min)
Immediately Dangerous to Health	300 ppm

Symptoms by Level

- **25-50 ppm:** Mild eye and nose irritation
- **50-100 ppm:** Headache, nausea, tearing
- **300 ppm:** Severe respiratory distress (IDLH)
- **>500 ppm:** Pulmonary oedema

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HEALTH HAZARDS, EXPOSURE LIMITS & FIRST AID

First Aid – By Route of Exposure

- **Eye Contact**
Flush with large amounts of water for at least 15-20 minutes. Seek immediate medical attention. Do not rub eyes.
- **Skin Contact**
Remove contaminated clothing. Wash skin thoroughly with water for 15 minutes. Treat for chemical burns if blistering occurs.
- **Inhalation**
Move victim to fresh air immediately. Administer oxygen if available. Call emergency services. Do not re-enter without SCBA.

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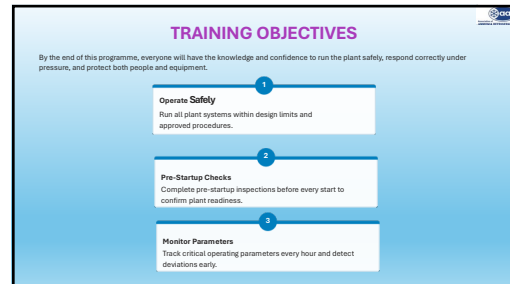
INDUSTRIAL APPLICATIONS OF AMMONIA REFRIGERATION

Cold Storage & Food	Ice Plants	Dairy & Beverage	Pharmaceutical & Chemical
Large-scale warehouses, blast freezers, and food processing facilities rely on NH ₃ for precise temperature control from -40 °C to +10 °C.	Block ice, flake ice, and tube ice plants use NH ₃ evaporators for efficient, high-capacity ice production in fishing and food industries.	Milk chilling, cream separation and beverage carbonation all require consistent, hygienic refrigeration that NH ₃ systems reliably provide.	Precise temperature-controlled environments for API storage, chemical reactors, and fermentation processes are maintained using NH ₃ systems.

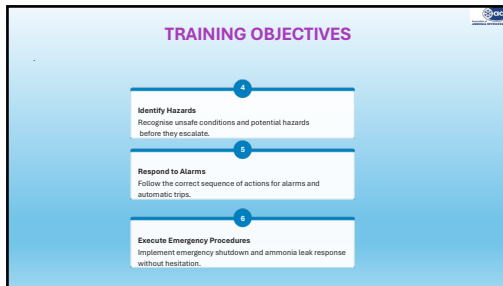
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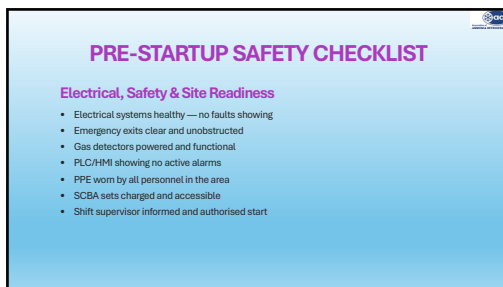
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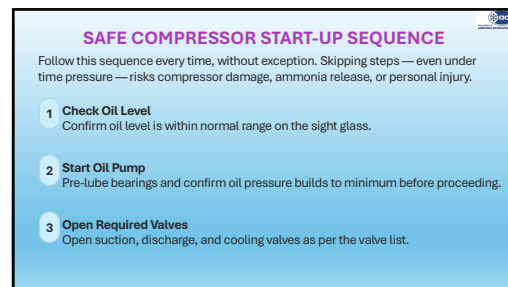
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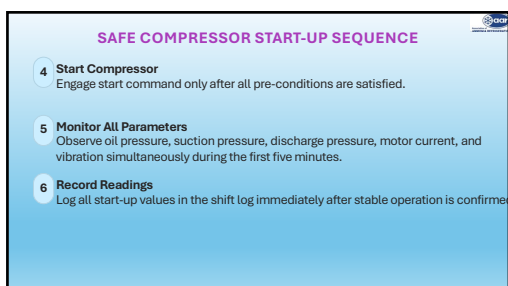
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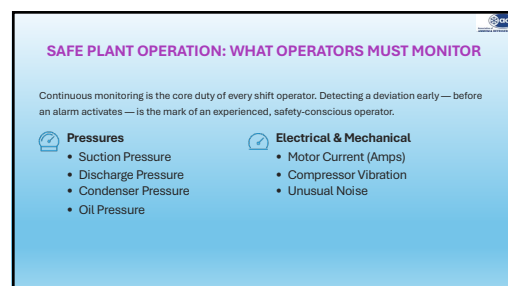
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SAFE PLANT OPERATION: WHAT OPERATORS MUST MONITOR

 Temperatures • Oil Temperature • Discharge Gas Temperature • Evaporator Temperature • Cooling Water Temperature	 Safety Systems • Ammonia Leak Detector Reading • Receiver Liquid Level • Active PLC Alarms
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SAFE COMPRESSOR & OIL SYSTEM OPERATION

Always Monitor

- Oil pressure above minimum operating value at all times
- Discharge temperature — stable and within normal range
- Motor current — stable, no sudden spikes
- No abnormal vibration or unusual mechanical noise
- No oil leakage from seals, flanges, or fittings

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SAFE COMPRESSOR & OIL SYSTEM OPERATION

Daily Oil System Checks

- Oil level on sight glass
- Oil filter differential pressure (DP)
- Oil cooler performance
- Oil temperature within specification

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SAFE COMPRESSOR & OIL SYSTEM OPERATION

Never Do This

- Start compressor with suction valve closed
- Run compressor with low or uncertain oil level
- Bypass, defeat, or ignore trip functions
- Continue running with abnormal vibration
- Ignore a rising oil filter DP — change the filter

⚠ Poor oil management causes bearing failure, rotor damage, and compressor seizure — all costly and avoidable.

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CONDENSER, RECEIVER & PUMP SAFE OPERATION

These three systems are critical links in the refrigeration cycle. Each requires specific monitoring disciplines to prevent high-pressure events, liquid carryover, and pump damage.

Condenser

- Confirm cooling water flow or fan operation before every shift
- Monitor condensing pressure — rising pressure signals fouling or water loss
- Check approach temperature to detect scaling or non-condensables
- Respond to high-pressure alarms immediately
- Follow the routine cleaning schedule without delay

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CONDENSER, RECEIVER & PUMP SAFE OPERATION

Receiver

- Check liquid level — never allow overfilling
- Monitor receiver pressure against normal operating range
- Inspect safety valve and level indicator visually each shift
- Check for abnormal frost patterns that indicate a leak
- Report any leakage from fittings or connections immediately

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CONDENSER, RECEIVER & PUMP SAFE OPERATION

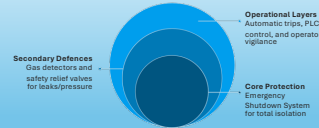
Pumps

- Confirm correct rotation direction after any maintenance
- Check mechanical seal for leakage during every round
- Monitor bearing temperature — elevated temp signals inadequate lubrication
- Listen for unusual noise or vibration
- **Never run pumps dry** — cavitation causes rapid seal and bearing damage

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PLANT SAFETY LAYERS: DEFENCE IN DEPTH

No single safety device protects the plant. Safety is achieved through multiple independent layers — each one acting as a backstop if the layer above it fails. Operators are the first and most important layer.



When an operator is alert and follows procedures, downstream safety systems rarely need to activate. Bypassing or ignoring any layer eliminates that protection for everyone on site.

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ALARM RESPONSE & SHIFT MONITORING

Every Hour — Record These Values

- Suction & discharge pressure
- Condensing pressure
- Oil pressure & temperature
- Motor current (Amps)
- Receiver liquid level
- Ambient temperature
- Leak detector status (ppm reading)

Trend analysis across shifts reveals developing faults before alarms activate. A rising oil temperature over three consecutive readings is a warning — not just a number.

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ALARM RESPONSE & SHIFT MONITORING

Alarm Response Protocol

Identify the alarm

Read the HMI alarm description carefully — do not guess.

Verify the instrument

Confirm the reading is genuine, not a sensor fault.

Inspect the equipment

Go to site — look, listen, and smell for abnormalities.

Take corrective action

Follow the relevant SOR. Do not improvise.

Inform supervisor & log event

Every alarm must be recorded with the time, cause, and action taken.

⚠️ **Never acknowledge and ignore an alarm. Every alarm is a symptom of a real condition.**

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SAFETY – ELECTRICAL

- Almost 90% of fire accidents are mainly due to electrical abnormalities
- Standard codes to be followed while selecting electrical equipment's
- Electrical PPE should be available such as Rubber mats, Gloves, Testers, safety shoes etc.



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AMMONIA LEAK DETECTION SYSTEM



There are two leaks in NH₃ system.
Vapor Leaks & Liquid Leaks.

Vapor leaks can occur in high-side components (piping, valves, compressors, flanges, etc.) and low-side components operating above atmospheric pressure.

Liquid ammonia leaks are from the mainly low-side components such as NH₃ pumps.

Ammonia detectors are recommended for personnel and property protection.

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OPERATOR'S GOLDEN RULES

These ten rules govern every decision an operator makes on shift. They are non-negotiable — no exception, no excuse, no override.

- 1 Safety before production
- 2 Never bypass interlocks
- 3 Verify before starting
- 4 Respond immediately to alarms
- 5 Record all abnormalities

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OPERATOR'S GOLDEN RULES

- 6 Stop work if unsafe
- 7 Report all leaks — even small ones
- 8 Follow SOPs at all times
- 9 Use PPE at all times in hazardous areas
- 10 Ask if unsure — never assume

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INTRODUCTION TO HAZOP

What Is HAZOP?

Hazard and Operability Study (HAZOP) is a systematic and structured risk assessment technique used to identify potential hazards, operational problems, and deviations from the intended design before and during plant operation.

It helps ensure that the plant operates **safely, efficiently, and reliably** by identifying risks and implementing appropriate safeguards.

What HAZOP Does

- Identifies credible hazards in every part of the process
- Identifies operability problems that cause downtime or unsafe conditions
- Evaluates whether existing safeguards are adequate
- Generates specific, trackable recommendations for improvement

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INTRODUCTION TO HAZOP

Why It Matters

- Prevents ammonia releases and accidents before they occur
- Improves plant reliability and reduces unplanned downtime
- Enhances emergency preparedness across the team
- Meets regulatory and corporate process safety requirements
- Captures and preserves operating experience from the plant floor

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THE HAZOP PROCESS & TEAM

Who Participates?

- **HAZOP Leader**
Facilitates the study — independent and trained in HAZOP methodology.
- **Process & Operations Engineers**
Provide technical and practical plant knowledge.
- **Maintenance, Instrumentation & Electrical**
Assess equipment reliability and control system safeguards.
- **HSE Representative**
Ensures regulatory compliance and risk assessment rigour.
- **Operations Representative**
The operator's voice — critical for realistic cause-and-consequence analysis.

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THE HAZOP PROCESS & TEAM

Required Documents

- PFD — Process Flow Diagram
- P&ID — Piping & Instrumentation Diagram
- Equipment Datasheets
- Cause & Effect Diagram
- Control Philosophy
- Alarm & Trip List
- Operating Procedures
- Emergency Procedures

Without current, accurate P&IDs, a HAZOP cannot be completed reliably. Always verify documents are as-built before the study begins.

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HAZOP METHODOLOGY: GUIDE WORDS & PARAMETERS

The HAZOP team works node by node through the plant, applying standard guide words to each process parameter to generate deviations — then asking “what causes this?” and “what happens as a result?”

Parameters Reviewed

Pressure	Temperature
Flow	Level
Composition	Phase
Speed	Power

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HAZOP METHODOLOGY: GUIDE WORDS & PARAMETERS

Guide Words & Examples

Guide Word	Meaning	Example Deviation
No	None of the intent	No Flow
More	Quantitative increase	High Pressure
Less	Quantitative decrease	Low Flow
Reverse	Opposite direction	Reverse Flow
As Well As	Additional component	Contamination
Other Than	Complete substitution	Wrong Material
Part Of	Partial intent achieved	Partial Flow

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HAZOP CASE STUDIES: COMPRESSOR, CONDENSER & RECEIVER

These worked examples show how the HAZOP process turns a simple deviation into a structured action. Operators should recognise every one of these scenarios from their own experience on the plant floor.

Compressor — Low Suction Pressure

Causes: Low refrigerant charge · Blocked suction filter · Closed suction valve
Consequences: Compressor trip · Loss of cooling · Equipment damage
Safeguards: Low-pressure alarm · Automatic trip · Routine inspection

Receiver — High Liquid Level

Causes: Expansion valve failure · Pump failure · Operator error on liquid management
Consequences: Liquid carryover to compressor · Compressor damage · Relief valve operation
Safeguards: Level transmitter · High-level alarm · High-high automatic trip

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HAZOP CASE STUDIES: COMPRESSOR, CONDENSER & RECEIVER

Condenser — High Condensing Pressure

Causes: Cooling water failure · Dirty condenser tubes · Fan failure · Non-condensable gases
Consequences: High-pressure trip · Relief valve lifting · Production loss
Recommendations: Regular cleaning · Fan PM schedule · Air purging procedure

Evaporator — Low Temperature

Causes: Incorrect control setpoint · Low product load · Expansion valve malfunction
Consequences: Product freezing · Coil icing · Reduced system efficiency
Recommendations: Verify control settings · Inspect valves · Monitor temperatures every hour

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RISK ASSESSMENT, SAFEGUARDS & ACTION TRACKING

Existing Plant Safeguards

Pressure Relief Valves

Last line of defence against overpressure — must be inspected and tested on schedule.

Gas Detectors & ESD

Continuous monitoring triggers automatic plant shutdown on confirmed ammonia release.

PLC Interlocks & Trips

High-pressure, low-oil-pressure, and temperature trips protect equipment automatically.

Preventive Maintenance & Training

The most cost-effective safeguards — scheduled maintenance prevents unplanned failures.

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RISK ASSESSMENT, SAFEGUARDS & ACTION TRACKING

HAZOP Recommendation Tracking
Every HAZOP recommendation must be tracked to closure. No recommendation should be left open without a documented status update.

Field	Required
Recommendation type	Engineering / Procedural / Training
Action owner	Named individual responsible
Due date	Agreed completion date
Status	Open / In Progress / Closed
Verification	Signed off by HAZOP leader

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CASE STUDY: AMMONIA LEAK FROM COMPRESSOR SHAFT SEAL

This is a real-world scenario. Work through it as a team — your experience and instincts as an operator are the most valuable input in this discussion.

Initial Indication Operator notices sharp ammonia odour during routine rounds	Root Cause Mechanical shaft seal has deteriorated due to wear and age. Seal was not included in the last PM
Immediate Actions Alarm raised - Personnel evacuated from the area - SCBA donned - Isolation valve closed - Emergency team notified	Lessons Learned Shaft seal inspection added to PM schedule. Gas detector sensitivity threshold reviewed. Operator nose-detection credited as first warning. SOPs

☐ Discussion prompt: Have you ever detected a problem before an alarm activated? What did you do — and what would you do differently today?

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KEY TAKEAWAYS & NEXT STEPS

Safe operation of an ammonia refrigeration plant is not complicated — but it requires discipline, vigilance, and respect for the hazards involved. Every operator who completes this training carries a responsibility to apply these principles every shift, every day.

Operate by the Rules Follow SOPs, complete checklists, record readings, and never by	Monitor Continuously Hourly readings and trend analysis are how experienced operators catch faults before they become emergencies.
Respond — Don't React Know your alarm response and emergency procedures so well that you act calmly and correctly under pressure.	Contribute to HAZOP Your operational experience is invaluable. Report near misses, participate in HAZOP reviews, and verify that actions are closed out.


 Apply Today


 Report Near-Miss


 Join Safety Review

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Thank You

Questions & Discussion

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